

An Equation of State in Analytical Form

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In most of the text-books of physical chemistry which insert a table of van der Waals' constants a and b , no example of their actual evaluation is given, and students often fall into misconception that the constants are uniquely determinate from the original and its two derived equations at critical points. Concretely speaking, from these equations we obtain $b = V_c/3 = RT_c/8p_c$ by substituting for V_c in the former from van der Waals' critical factor, $RT_c/p_cV_c = 8/3$, and consequently $a = 27p_cb^2 = 3p_cV_c^2 = 27(RT_c)^2/64p_c$, whereas for real gases, these two expressions of b give inconsistent values, $V_c/3$ being always less than $RT_c/8p_c$. The latter however has been accepted to make

use of calculating molecular diameters.⁽¹⁾ To eliminate this inconsistency from van der Waals' equation, the following correction is needed:

$$b_{corr.} = b \left(\frac{3}{8} \frac{RT_c}{p_c V_c} \right) = \frac{V_c}{3} \left(\frac{3}{8} \frac{RT_c}{p_c V_c} \right) = \frac{RT_c}{8p_c},$$

where RT_c/p_cV_c in the correction factor is an actual critical factor, ranging from 3.23 to 3.97 for non-polar and larger slightly polar substances. Substitute $a_{corr.}$ for a corresponding to $b_{corr.}$, van der Waals' equation per mol. is

(1) e.g. Landolt-Börnstein I-1, 1950, p. 325.

[illegible]

Table 4

(2-ε) Values at Critical Points and Percentage Divergences of Approximate Formula $RT_c/p_c V_c = 2/3 \cdot (1 + 3V_c^{0.677})$ from Experimental Data

Substance	2-ε	A	Substance	2-ε	A	Substance	2-ε	A
He	1.931	+2.50	C ₅ H ₁₂	1.924	+0.52	CH ₃ SH	1.922	-0.57
Ne	1.935	+2.35	i-C ₅ H ₁₂	1.926	+1.55	C ₂ H ₅ SH	1.924	+0.85
A	1.925	+0.84	cyclo-C ₆ H ₁₄	1.931	+3.95	CH ₃ SCH ₃	1.920	-1.37
Kr	1.927	+1.63	C ₆ H ₁₄	1.924	+0.53	C ₂ H ₅ SC ₂ H ₅	1.933	+4.67
Xe	1.921	-0.89	C ₇ H ₁₆	1.923	+0.28	HCO ₂ CH ₃	1.905	-7.39
H ₂	1.936	+4.31	C ₈ H ₁₈	1.923	+0.78	HCO ₂ C ₂ H ₅	1.913	-5.02
N ₂	1.928	+1.93	Br ₂	1.932	+3.51	HCO ₂ C ₃ H ₇	1.917	-2.75
O ₂	1.925	+0.83	Hg	1.915	-2.28	CH ₃ CO ₂ CH ₃	1.909	-6.06
Cl ₂	1.921	-0.79	CS ₂	1.933	+4.42	CH ₃ CO ₂ C ₂ H ₅	1.912	-4.82
CO	1.931	+3.01	CCl ₄	1.927	+1.96	CH ₃ CO ₂ C ₃ H ₇	1.914	-4.29
CO ₂	1.918	-1.85	CHCl ₃	1.940	+9.81	CH ₃ CO ₂ CH ₂ CH(CH ₃) ₂	1.937	+7.02
CF ₂ Cl ₂	1.925	+0.96	CH ₃ OCH ₃	1.918	-2.13	C ₂ H ₅ CO ₂ CH ₃	1.913	-4.34
COCl ₂	1.933	+4.31	CH ₃ OC ₂ H ₅	1.922	-0.62	C ₂ H ₅ CO ₂ C ₂ H ₅	1.915	-3.58
N ₂ O	1.908	-5.43	C ₂ H ₅ OC ₂ H ₅	1.922	-0.57	C ₃ H ₇ CO ₂ CH ₃	1.917	-2.82
PH ₃	1.915	-3.13	C ₂ H ₅ OC ₃ H ₇	1.926	+1.41	(CH ₃) ₂ CHCO ₂ CH ₃	1.912	-2.12
SO ₂	1.908	-5.93	C ₂ H ₅ Cl	1.926	+1.16	C ₃ H ₇ CO ₂ C ₂ H ₅	1.932	+4.63
SnCl ₄	1.927	+2.06	C ₆ H ₅ CH ₃	1.927	+1.87	(CH ₃) ₂ CHCO ₂ C ₂ H ₅	1.937	+7.08
CH ₄	1.927	+1.64	C ₆ H ₆	1.922	-0.49	C ₂ H ₅ NH ₂	1.921	-0.82
C ₂ H ₆	1.923	-0.12	C ₆ H ₅ F	1.920	-1.00	(C ₂ H ₅) ₂ NH	1.922	-0.59
C ₂ H ₄	1.927	+1.48	C ₆ H ₅ Cl	1.923	-0.02	(C ₂ H ₅) ₃ N	1.934	+5.74
C ₂ H ₂	1.915	-2.91	C ₆ H ₅ Br	1.921	-0.78	(CH ₃) ₂ CHCH(CH ₃) ₂	1.926	+1.46
C ₃ H ₈	1.921	-1.00	C ₆ H ₅ I	1.925	+1.01	(CH ₃) ₂ CHCH ₂ CH ₂ CH(CH ₃) ₂	1.926	+1.57

The mean of (2-ε) = 1.923 ± 0.008, the mean of A = ±2.6%.

written down:

$$p + \frac{a_{corr.}}{V^2} = \frac{RT}{V - b_{corr.}} \quad (1).$$

The validity of equation (1) can be tested simply by calculating $f = (p + a_{corr.}/V^2)(V - b_{corr.})/RT$ at different isotherms, which must be unity, if the equation holds good. As seen from Table 1, f deviates from unity as pressure moves slightly away from the critical pressure, so that equation (1) is valid only within narrow limits of pressures, though the range becomes wider as the increase in temperature.

Moreover mere trial for the evaluation of values of $(V - b_{corr.})$ with ordinary liquids at an ordinary temperature proves that the applicability of equation (1) to liquids, should be rejected since all such values become negative (compare column 2 with column 3 in Table 2).

We have the pure thermodynamic equation

$$p + \left(\frac{\partial U}{\partial V} \right)_T = T \left(\frac{\partial p}{\partial T} \right)_V = T \frac{\alpha}{\beta} \quad (2),$$

where α and β denote thermal expansion coefficient and isothermal compressibility.⁽²⁾ If there exists an equation of state for liquids, the thermal pressure of which has the form $ART/(AV - b_{corr.})$,

A being a correction factor so as to let the denominator of thermal pressure of equation (1) be positive, the equality:

$$T \frac{\alpha}{\beta} = \frac{ART}{AV - b_{corr.}} \quad (3)$$

may be satisfied, if A is suitably chosen. Since R (82.06 cc.-atm./deg. mol.) and V (cc./mol.) are both referred to 1 mol. of gases, A may be or may not be proportional to the degree of non-polar association at T°K.

For test of this postulation, 21 kinds of liquids have been adopted from Henning's table.⁽³⁾ In Table 2 are given A's divided by $3RT_c/8p_c V_c$, from which we can conclude that A is in nearly the same magnitude with $3RT_c/8p_c V_c$, for ordinary liquids except acetone, alcohols and water, or in other words, for liquids having low dielectric constants relation (3) is transformed into

$$T \frac{\alpha}{\beta} = \frac{RT}{V - b} \quad (4).$$

In accord with the above correction for thermal pressure, an appropriate correction for cohesive pressure will be considered below.

As already known b decreases as V decreases,

(2) e.g. International Critical Tables IV, p. 19.

(3) F. Henning's "Warmetechnische Richtwerte", p. 17-19, 20-21.

and so the assumption of keeping b to be constant independent of V must yield deviation in thermal pressure, but the deviation therefrom can be attributed to a suitable correction of a in cohesive pressure.

Now assume $a^*_{corr.}$ to vary slightly with V and take the following form:

$$a^*_{corr.} = aV^\epsilon, \\ \epsilon = \text{a constant independent of pressure,}$$

then for substances having low dielectric constants it follows from (1), (3) and (4) that

$$p + \frac{a}{V^{2-\epsilon}} = \frac{RT}{V-b}, \\ a = 3p_c V_c^2, \quad b = V_c/3 \quad (5).$$

Adopting pv - values of gases from I. C. T.⁽⁴⁾ and Henning's table,⁽⁵⁾ we have calculated $(2-\epsilon)$ values for several gases. One of them is exemplified in Table 3.

As a whole, the constancy of $(2-\epsilon)$ values is fairly good over a wide range of pressures of each isotherm, though the constant range becomes restricted as the temperature decreases. The variation of $(2-\epsilon)$ values with temperature is similar for all the examined gases except He, their values increasing from a value less than 1.92 to a value slightly greater than 2. Inserting the mean value of $(2-\epsilon)$ at each isotherm in equation (5), we can obtain the equation of state at respective temperature. The thus analytically determinate equation is, therefore, more reasonable and accurate than a usual equation of algebraic form: $pV = a_0 + a_1/V + a_2/V^2 + a_3/V^3 + \dots$.

Besides the gases above examined, all gases and liquids with known critical-point data except those having high dielectric constants take a universal value, 1.923 ± 0.008 , for $(2-\epsilon)$ at critical points (see Table 4).

The following are three formulae at the critical point which can be derived from the new equation of state.

The criteria generally used to determine whether or not any equation of state holds good are $RT_c/p_c V_c$, T_B/T_c (T_B = Boyle point) and $T_c/p_c \cdot (dp/dT)_c$. These are of course physico-chemical constants giving the values close to 3.7, 2.6 and 7.0 respectively but none of the proposed equations gives concordant values simultaneously.

Inserting $a = 3p_c V_c^2$ and $b = V_c/3$ in equation (5) at the critical point, and rearranging them, it follows that

$$\frac{RT_c}{p_c V_c} = \frac{2}{3} (1 + 3V_c^\epsilon) \quad (6),$$

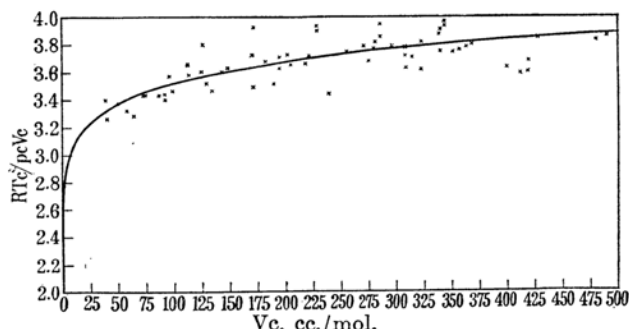


Fig. 1.—Relation between $RT_c/p_c V_c$ and V_c for low dielectric substances.

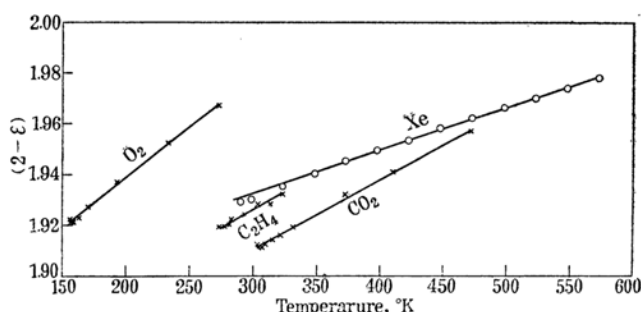


Fig. 2.—The temperature dependence of $(2-\epsilon)$ for some gases.

here of course ϵ is its value at the critical point and V_c is expressed in cc.

Firstly, if we take the mean of ϵ from the results summarized in Table 4, relation (6) becomes

$$\frac{RT_c}{p_c V_c} = \frac{2}{3} (1 + 3V_c^{0.077}) \quad (7),$$

which serves as an approximate formula. d 's in Table 4 denote the percentage divergences from experiments and their mean value becomes ± 2.6 %. Also the relation between $RT_c/p_c V_c$ and V_c is diagrammatically shown in Fig. 1, in which the curve is plotted by formula (7). Quite recently Himpan⁽⁶⁾ put forward the empirical formula, $RT_c/p_c V_c = 2.92 + 1/3 \cdot \log(nM)$, where M is the molecular weight and n the degree of association, but its graphical test has shown that his formula is worse than formula (7).

Secondly, since the Boyle temperature is much higher than the critical temperature, relation $T_B = b/aR = 9p_c V_c/R$ derived from the van der Waals' equation may be allowable. Using this relation in conjunction with formula (7), there results

$$\frac{T_B}{T_c} = \frac{27}{2(1 + 3V_c^{0.077})} \quad (8).$$

(4) International Critical Tables III, p. 4-19, 248-249.

(5) F. Henning, l.c., 34-40.

(6) J. Himpan, Z. Physik, 131, 17 (1951).

Formula (8) gives concordant values with experiments: 2.70 (2.70), 2.60 (2.73), 2.58 (2.59), 2.57 (2.59), 2.56 (2.58) for Ne, A, N₂, CO, CH₄ respectively, the values in parentheses being the observed values.⁽⁷⁾

Thirdly, write equation (5) in the form

$$p = \frac{RT}{V-b} - \frac{a}{V^{2-\varepsilon}},$$

and differentiate with respect to T , remembering ε to be dependent on temperature,

$$\left(\frac{dp}{dT}\right)_V = \frac{R}{V-b} - \frac{a}{V^2} V^\varepsilon \log_e V \cdot \frac{d\varepsilon}{dT}.$$

Putting this in the thermodynamic relation, $(dp/dT)_c = [dp/dT]_{T=T_c}$, we readily obtain

$$\frac{T_c}{p_c} \left(\frac{dp}{dT}\right)_c = \frac{3RT_c}{2p_c V_c} - 3T_c V_c^\varepsilon \log_e V_c \cdot \left(\frac{d\varepsilon}{dT}\right)_c,$$

or replace from formula (7), it follows that

$$\begin{aligned} \frac{T_c}{p_c} \left(\frac{dp}{dT}\right)_c &= 1 + 3V_c^{0.677} - 3 \\ &\times 2.303T_c V_c^{0.677} \log_e V_c \left(\frac{d\varepsilon}{dT}\right)_c \end{aligned} \quad (9).$$

For example take CO₂ for which $T_c = 304.2^\circ\text{K}$., $V_c = 44.01/0.460$ cc., $\varepsilon = 0.082$ and $T_c/p_c \cdot (dp/dT)_c = 7.14^{(8)}$ are given, $(d\varepsilon/dT)_c$ is evaluated to be -0.00029 , or -0.00032 by the use of formula (9). These values agree well with the experimental value, $-(0.00028 \pm 0.0004)$, which has been obtained from the mean of $(2-\varepsilon)$ values at several isotherms: 1.912 (30.98°C., critical temperature), 1.916 (48.10°C.), 1.919 (57.75°C.), 1.935 (100°C.), 1.946 (137°C.), 1.969 (198°C.), 1.972 (258°C.).

As already stated, $3RT_c/8p_c V_c$ corresponds to the molecular association factor A at the critical point, so it follows from formula (6) that

$$A = (1 + 3V_c^\varepsilon)/4$$

The numerical values of A lie from the lowest value of 1.22–1.29 for non-polar molecules such as Ne, He, A, Kr, N₂ and CO to the highest value of 1.47–1.49 for alkyl esters such as CH₃CO₂CH₃, CH₃CO₂C₂H₅ and CH₃CO₂C₃H₇. Although the former value, to whose class Br₂ and Hg belong, may be inconsistent with ordinary physico-chemical knowledge of so-called normal liquids, yet it may be rather conceivable that non-polar association takes place at the critical point where gaseous and liquid states begin to coexist undoubtedly in a molecular aggregation different from the gaseous state, and that such association in the case of normal liquids may keep nearly

constant for a wide range, from critical to ordinary temperatures.

Summary

(1) An equation of state in analytical form is proposed:

$$p + \frac{a}{V^{2-\varepsilon}} = \frac{RT}{V-b}, \quad a = 3p_c V_c^2, \quad b = V_c/3.$$

Values of $(2-\varepsilon)$ keep constant over a wide range of pressures of each isotherm. Taking the mean of $(2-\varepsilon)$ values at each isotherm, we obtain an equation of state which is more reasonable and accurate than the usual isothermal equation of algebraic form.

(2) Tests made with 66 kinds of substances having low dielectric constants prove that values of $(2-\varepsilon)$ at critical points are universal to give 1.923 ± 0.008 .

(3) The following three formulae at the critical point are derived from the new equation in which V_c is expressed in cc./mol.

$$(i) \quad \frac{RT_c}{p_c V_c} = \frac{2}{3} (1 + 3V_c^{0.677}),$$

$$(ii) \quad \frac{T_B}{T_c} = \frac{27}{2(1 + 3V_c^{0.677})},$$

$$(iii) \quad \frac{T_c}{p_c} \left(\frac{dp}{dT}\right)_c = 1 + 3V_c^{0.677} - 3 \\ \times 2.303T_c V_c^{0.677} \log V_c \cdot \left(\frac{d\varepsilon}{dT}\right)_c.$$

The first formula is concordant with $\pm 2.6\%$ average divergence for 66 kinds of low dielectric substances and the two following are also equally concordant with the experimental data.

Addendum

The constancies of ε were found to be fairly good over a wide range of pressures at each isotherm. Their dependence on temperature, however, was left unsaid since there are but few favorable data from which a conclusion can be deduced.

Quite recently Beattie, Barriault and Brierley⁽²⁾ reported on the compressibility measurements for gaseous xenon from the critical temperature to 300°C and over the density range of from 1 to 10 mol. per liter, and so by making use of their results we have had an opportunity to certify the linearity between ε and temperature which was already suggested in the case of CO₂.

For xenon we put $b = 40.06$ cc. and $\log a = 6.3993891$ calculated from their newly determined critical constants, $p_c = 57.89$ atm., $d_c = 8.32$ mol./liter, $T_c = 16.65^\circ\text{C} + 273.13$. The $(2-\varepsilon)$ values at every 50°C intervals from 25 to 275°C. are listed

(7) Adopted from E. A. Guggenheim's "Thermodynamics", p. 140.

(8) Adopted from S. Mizushima's "Physical Chemistry", III, p. 645.

(1) J. A. Beattie, R. J. Barriault, J. S. Brierley, *J. Chem. Phys.*, **19**, 1219 (1951).

Table 5
(2-ε) for Xenon

mol./liter	(2-ε)					
	25°C.	75°C.	125°C.	175°C.	225°C.	275°C.
10.0	1.934	1.942	1.951	1.960	1.968	
9.0	1.935	1.942	1.951	1.959	1.968	1.977
8.0	1.934	1.942	1.951	1.959	1.967	1.976
7.0	1.932	1.941	1.950	1.958	1.967	1.975
6.0	1.930	1.940	1.949	1.957	1.966	1.974
5.0	1.928	1.939	1.948	1.957	1.965	1.973
4.0	1.926	1.938	1.947	1.956	1.964	1.972
3.0	1.926	1.937	1.947	1.955	1.963	1.971
2.0	1.927	1.938	1.948	1.956	1.964	1.972
1.0	1.931	1.942	1.951	1.959	1.966	1.974
Mean	1.930	1.940	1.949	1.958	1.966	1.974

Table 6
Percent Deviation from Experiments

mol./liter	100 (p _{calc.} - p _{obs.})/p _{obs.}					
	25°C.	75°C.	125°C.	175°C.	225°C.	275°C.
8.0	-6.52	-1.66	-0.824	-0.396	-0.406	-0.473
7.0	-2.93	-1.35	-0.424	-0.073	-0.158	-0.164
6.0	-0.11	-0.10	-0.028	+0.163	+0.079	+0.024
5.0	+1.562	+0.525	+0.288	+0.377	+0.280	+0.213
4.0	+2.095	+0.805	+0.442	+0.493	+0.378	+0.328
3.0	+1.736	+0.724	+0.419	+0.443	+0.371	+0.321
2.0	+0.864	+0.346	+0.184	+0.259	+0.225	+0.205
1.0	-0.121	-0.162	-0.151	-0.034	-0.005	-0.011
Mean	1.99	0.709	0.345	0.258	0.228	0.217
(Beattie-Bridgeman's equation)	1.37	0.282	0.424	0.294	0.171	0.190

in, Table 5, and the percent deviations, 100 (p_{calc.} - p_{obs.})/p_{obs.}, from 1 to 8 mol. per liter, in Table 6. As seen from these tables, the constancies of (2-ε) at respective isotherms are quite satisfactory and the average percent deviations are as small as those of the Beattie-Bridgeman equation of state (the last line in Table 6).

The variation of (2-ε) with temperature is diagrammatically shown in Fig. 2, in which are also plotted those of CO₂, C₂H₄ and O₂ which were computed from the compressibility data already mentioned.

As to xenon, (2-ε) is strictly a straight line over the whole range of temperatures. This relationship appears to be equally well for the other gases as judged from their graphical

representations. So that we can conclude that the linearity:

$$\epsilon = \epsilon_c + c(T - T_c), \quad \epsilon_c, c = \text{const.}$$

holds true so far as the present data are concerned. Here ϵ_c is not ϵ at the critical point but the mean at the critical isotherm.

The author is indebted to SCAP CIE at Sasebo for having made him possible by mail from Tokyo to read the Journal of Chemical Physics, October, 1951, in which Beattie, Barriault and Brierley published their compressibility measurements for xenon.

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